Claims 1-5 (previously canceled)

Claim 6 (currently amended) A process for obtaining [polyglycolyl] urea hydantoin resin from aromatic diglycinates for insulating electric conductor, in the absence of HCN polluting residues, comprising the following steps:

a) reacting a mixture of methylhaloester and [diamine] methylenedianiline in a $C_1$ - $C_4$ aliphatic solvent under reflux conditions at atmospheric pressure and up to solvent reflux temperature, wherein said methylhaloester is selected from the group consisting of methyl- bromopropionate and methylchloropropionate;

b) adding a catalyst to the reaction mixture to obtain diglycinate in solution;

c) separating the solvent through atmospheric distillation;

d) crystallizing the diglycinate;

e) filtering and purfying the diglycinate by washing with water;

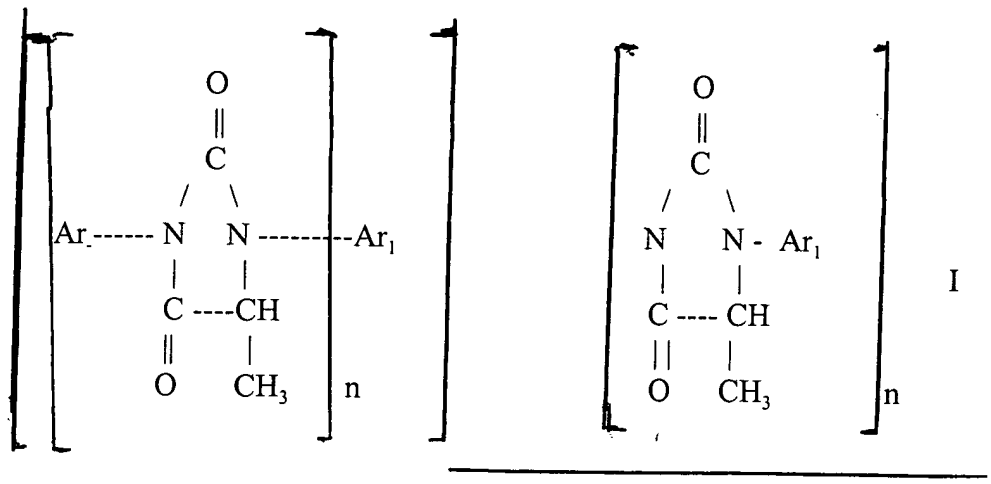
f) drying the methyl diglycinate obtained;

g) reacting the obtained diglycinate with cresylic acid in a reactor until solution is complete;

h) stirring the diglycinate with [aromatic] a methylene diisocyanate [ isocyanate], solvent and catalyst;

i) distilling and then cooling the reaction product; and

j) recovering the [polyglycolyl] urea hydantoin resin having the formula:



I

where $Ar_1$ is a substituted aromatic compound or a substituted diphenylalkyl, and $2<n<500$.

Claim 7 (previously added) The process according to claim 6, wherein the methylhaloester is selected from the group consisting of methylbromoproprionate and methylchloropropionate.

Claim 8 (previously added) The process according to 6, wherein the diamine is methylenedianiline.

Claim 9 (currently amended) The process according to claim 6, wherein the mixture reflux is conducted for [16] 19 hours.

Claim 10 (previously added) The process according to claim 6, wherein the catalyst is triethylamine.

Claim 11 (previously added) The process according to claim 10, wherein the triethylamine is added at a rate of 0.178 l/hr per Kg of product during a 3-5 hour period.

Claim 12 ( canceled)

Claim 13 (previously added) The process according to claim 6, wherein the diglycinate is crystallized at 50° C.

Claim 14 (currently amended) The process according to claim 6, wherein the [stirring with] methylene diisocyanate is stirred at a temperature of 60 C.

Claim 15 (currently amended) The process according to claim 6 [wherein the] further comprising adding triethylenediamino or1,4 diazobicyclo (2,2,2) octane catalyzer [catalyst is added] after step h, at a temperature of up to 180C.

Claim 16 (currently amended) The process according to claim [6] 15, [wherein the distilling] further comprising performing distillation [is conducted] at a temperature of 200 C.

Claim 17 ( currently amended) The process according to claim 6, wherein the cooling is conducted at $70^0$ C.

Claim 18 (currently amended) The process according to claim 6 wherein the product has a viscosity of 44 to 47 seconds a 25 C, as determined in a No. 4 Ford Cup on a polymer sample..

Claim 19 (previously added) The process according to claim 6, wherein the catalyst in step (h) is selected from the group consisting of triethylenediamino and 1,4 diazobicyclo (2,2,2) octane.

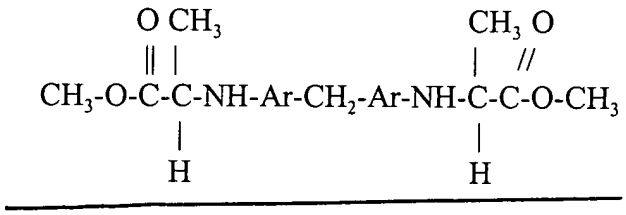
Claim 20 (currently amended) The process according to claim 6 wherein the polyglycolyl urea hydantoin obtained has a viscosity (Cp) of 4,800 at 15% solids at 70 C.

Claim 21 (previously added) The process according to claim 6, wherein the $C_1$ - $C_4$ aliphatic solvent is methanol.

Claim 22. (previously added) The process according to claim 6, wherein the reflux temperature of the $C_1$ - $C_4$ aliphatic solvent is 58 - 63° C.

Claim 23 (currently amended) The process according to claim 6, wherein the methyl methyl diglycinate obtained is dried with hot air at 40 C and corresponds to a sterioisomer mixture with a melting point of 95-116 C, of the following formula II:

II $[\ [Ar_1[NH\text{-}(CH_3)\text{ - }COOCH_3]_2]\ \ \underline{Ar_1[NH\text{-}CH(CH_3)\text{- }COOCH_3]_2}\ ]$



wherein Ar is an aromatic compound.

24) (previously canceled)

25) (canceled)